| Question | Proforma | Criteria | Торіс | Question | Date question asked | Date response required | Date received | | Confidenti |
|----------|-------------------------|----------|-------|---|---------------------|------------------------|---|---------------------|------------|
| No. | section | | | | | | | to Question # | al (y/n) |
| | 1 3.3.1 | (a.iii) | | It appears that the financial and carbon assessments use baselines that differ (maximising the apparent benefit of each aspect).[1] In order to provide greater clarity could the BAU, Heat Pump and H2 deployment scenarios be shown on a consistent basis? | 23 August 2016 | 25 August 2016 | 02 September 2016 | | |
| | 2 3.3.1 | (a.iii) | | The fall in the levelised cost of hydrogen is a critical driver of the benefit estimate as shown in Table B4. In particular Bio-SNG which is itself in infancy. Can it be clarified how the risks associated with this source of hydrogen have been accounted for in the assessment of benefits. | 23 August 2016 | 25 August 2016 | 03 September 2016 | | |
| 3 | 3 3.3.1 | (a.iii) | | Can it be clarified how net benefits have been derived? In particular, what assumptions are made about additional R&D costs, what system wide costs would be incurred (eg for full H2 deployment -Dodds and Demoullin estimated conversion costs of £500 per household). Could the levelised costs be used to show analogous figures. | 23 August 2016 | 25 August 2016 | 04 September 2016 | | |
| | 4 3.3.1 | (a.iii) | | Cost/carbon savings are based on 10% and 20% hydrogen blends- is there a risk that 10% may not be achievable once appliance testing etc. is conducted? "avoidance of network reinforcement otherwise required" is included in cost savings. Should it not be acknowledge that network reinforcement may be needed for reasons other than heat pump deployment i.e. electrification of vehicles? | 23 August 2016 | 25 August 2016 | 05 September 2016 | | |
| 1 | 5 2.3.3 (p11) | General | | Does the 'accredited by Ofgem' reference under composition measurement and CV refer to what you are looking for a view from Ofgem on in section 7 of your submission? | 25 August 2016 | 31 August 2016 | 06 September 2016 | | |
| (| 5 Section 7 | General | | While we may have a view on the use of declared vs determined CV, does Ofgem have a formal role to approve the choice taken by NGGD? Broadly, what does the process for this look like and what are the timings be? | 25 August 2016 | 31 August 2016 | 07 September 2016 | | |
| ; | 7 General | g | | Please can you provide more information on what are the main the issues that need to be addressed for hydrogen to safely blended and used on the distribution network? This should be in the form of a chart/checklist including evidence required by HSE. If there are differences if the NTS is used please highlight those too. | 09 September 2016 | 15 September 2016 | 30-Sep (Verbally), 04- Oct (Written) | | |
| 5 | 3 Appendix J | b | | The cost of buying and installing an electrolyser onsite makes up a large sum of the cost of the project. (i) Why does hydrogen need to be produced by an electrolyser onsite rather than shipped in? (ii) Could the electrolyser be rented rather than bought? Please could you provide the costs of renting, if that is possible, compared to buying the electrolyser. Alternatively can it be purchased second hand? Is possible, please provide the cost of a second hand electrolyser and it's expected lifetime. (iii) Can you provide costings and risk assessment of having hydrogen brought and used from a safe place on the campus, compared to procuring and using an electrolyser onsite. | 09 September 2016 | 15 September 2016 | 30-Sep (Verbally), 04- Oct (Written) | | |
| 9 | 8.2 | g | | (i) Please can you provide a high level customer engagement plan that will be used for customers onsite and the learning taking from Oban? (ii) Please can you include as an explicit project deliverable, the consolidation of work and learning on customer engagement for future trails of hydrogen on the public network? | 09 September 2016 | 15 September 2016 | 30-Sep (Verbally), 04- Oct (Written) | | |
| 10 | D Appendix C (C.2.3) | b | | Part of the project plan identifies that a 6" steel pipe must be inspected. (i) Why does this pipe need to be inspected? Would the inspection be needed if the project doesn't go ahead? (ii) What is the mitigation if repairs are needed to the pipe? Are these costs included in the project cost? Given its depreciated cost vs new asset life should Keele make a contribution if it is replaced. | 09 September 2016 | 15 September 2016 | 30-Sep (Verbally), 04- Oct (Written) | | |
| 1: | l General | а | | Please can you provide more detail on: (i) The business case for biohydrogen as source (ii) The long-term cost of the production of biohydrogen compared to the cost of natural gas, given learnings over the last year and also allowing for different scenarios for gate fees. | 09 September 2016 | 15 September 2016 | 30-Sep (Verbally), 04- Oct (Written) | | |

Gas Network Innovation Competition Full Submission <u>Supplementary Answer Form</u>

Project: HyDeploy

Tick if this answer has been provided verbally: \Box

| Project code | NGGDGN03/1 | Question Number | 1 |
|---|--|---|--|
| Question date | 230816 (delivered 310816) | Answer date | 020916 |
| Submission section question relates to | 3.3.1 | · | |
| Торіс | Benefits | | |
| Question | It appears that the financial and ca that differ (maximising the apparen order to provide greater clarity cou deployment scenarios be shown on | nt benefit of each asp Ild the BAU, Heat Pun | ect).[1] In |
| Notes on question | [1] Financial benefits: In section 3.3 a the difference between levelised costs of business as usual –so an incremental d analytical view this 'hides' the financial benefit of the project then emerges from is dependent on other technology). Ca relation to BAU so are on a different ba See also eg page 59. | of air source heat pump lifference in costs is use performance relative to m a sharply falling H2 o rbon benefits: are meas | s and d. From the b BAU. The cost (but this sured in |

| Answer | The UK has national commitments to carbon savings, and to do so requires de-carbonisation of heat. |
|-------------|---|
| | Both heat pumps and hydrogen deliver substantial carbon savings relative to business as usual. However, hydrogen not only does so with less disruption to consumers, but also at lower cost. |
| | The overarching approach taken was to evaluate the costs and carbon emissions for the scenarios, and therefore to present the benefits. |
| | Appendix B of the submission, particulary p59, provides: |
| | The absolute costs of decarbonisation via heat pumps as well as the additional costs compared with fossil gas boilers The absolute carbon intensity of heat delivered by hydrogen as well as the carbon savings relative to fossil gas boilers |
| | However, it is recognised that we didn't show the absolute or relative carbon intensity of heat delivered by heat pumps. This was calculated, but not provided and is required for completeness. The table below shows all the data on a consistent basis as absolute values as well as relevant comparisons |
| | This shows that both hydrogen and heat pump deliver very similar levels of carbon savings, but the hydrogen route is substantially lower cost compared with heat pumps. Not only is it therefore a much less disruptive solution for the gas customer compared with heat pumps, it does so at lower cost; this is the saving shown in the submission. |
| Attachments | See Table below |

| Heat | es for GB at 20% (Method 1) Heat displaced | TWh pa | 0.0 | To 2030 | 29.0 | 29. |
|--|---|--|--|--|---|---|
| | | i wn pa | 0.0 | 14.1 | 29.0 | 29 |
| Absolute Value | Levelised cost of heat | C/MWb | 50.2 | 62.0 | 62.0 | 62 |
| Fossil gas | | £/MWh | 59.2 | 62.8 | 63.9 | 63 |
| | Annual Cost | £M pa | 0 | 886 | 1,852 | 1,85 |
| | Cumulative Net Present Value by decade | £M (NPV) | 0 | 1,893 | 10,458 | 17,43 |
| | Carbon intensity (delivered heat) | kg/MWth | 232 | 228 | 228 | 22 |
| | Annual emissions | 000 te pa | 0 | 3,222 | 6,611 | 6,61 |
| heelute Value | Cumulative emissions by decade | 000 te | 0 | 10,287 | 69,104 | 135,21 |
| Absolute Value | Levelised cost of Heat (excl reinforcement) | £/MWh | 120.2 | 120.1 | 124.1 | 110 |
| | Annual Cost (inc reinforcement) | £M pa | 139.2 0 | 130.1 2,239 | 124.1 3,605 | 118 3,44 |
| | | £M (NPV) | 0 | 5,341 | | |
| Heat pumps | Cumulative Net Present Value by decade | | 85 | 5,341 29 | 23,694 15 | 36,98 |
| | Carbon intensity Annual emissions | kg/MWth 000 te pa | 0 | 408 | 428 | 4 |
| | | 000 te pa | 0 | 135 | 7,004 | |
| heelute Value | Cumulative emissions by decade | 000 te | 0 | 135 | 7,004 | 9,15 |
| Absolute Value | Levelised cost of heat | £/MWh | 142.1 | 107.2 | 104.4 | 10 |
| | Annual Cost | £/MWII £M pa | 143.1 0 | 107.3 1,514 | 104.4 3,025 | 101 2,95 |
| | | | 0 | | | |
| Hydrogen | Cumulative Net Present Value by decade Carbon intensity | £M (NPV) kg/MWth | 77 | 3,443 30 | 17,669 27 | 28,92 |
| | Annual emissions | 000 te pa | 0 | 30 430 | 774 | 65 |
| | | 000 te pa | 0 | 1,574 | 8,890 | |
| Somparisons | Cumulative emissions by decade | 000 te | 0 | 1,574 | 8,890 | 15,95 |
| Comparisons | Cumulative sources by best nume relative to feesil sec | 000 to | | 10 15 2 | 62 100 | 120.05 |
| Carbon | Cumulative savings by heat pump relative to fossil gas | 000 te | 0 | 10,152 | 62,100 | 126,05 |
| | Cumulative savings by hydrogen relative to fossil gas | 000 te £M (NPV) | 0 | 8,714 | 60,214 | 119,26 |
| | | | | 3,447 | 13,236 | 19,54 |
| Costs | Cumulative decarbonisation by heat pump relative to fossil gas | . , | | | | 44 40 |
| | Cumulative decarbonisation by hydrogen relative to fossil gas | £M (NPV) | 0 | 1,550 | 7,210 | |
| Costs Savings | | . , | | | | 11,48 8,06 |
| Savings | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump | £M (NPV) | 0 | 1,550 1,897 | 7,210 6,025 | 8,06 |
| Savings Absolute Value | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) | £M (NPV) £M (NPV) | 0 0 To 2020 | 1,550 1,897 To 2030 | 7,210 6,025 To 2040 | 8,06 To 205 |
| Savings Absolute Value Heat | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced | £M (NPV) | 0 | 1,550 1,897 | 7,210 6,025 | 8,06 To 205 |
| Savings Absolute Value Heat | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced | £M (NPV) £M (NPV) TWh pa | 0 0 To 2020 0.0 | 1,550 1,897 To 2030 7.1 | 7,210 6,025 To 2040 14.5 | 8,06 To 205 |
| Savings Absolute Value Heat | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat | £M (NPV) £M (NPV) TWh pa | 0 0 To 2020 0.0 59.2 | 1,550 1,897 To 2030 7.1 62.8 | 7,210 6,025 To 2040 14.5 63.9 | 8,06 To 205 14 |
| Savings Absolute Value Heat | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost | £M (NPV) £M (NPV) TWh pa £/MWh £M pa | 0 0 To 2020 0.0 59.2 0 | 1,550 1,897 To 2030 7.1 62.8 443 | 7,210 6,025 To 2040 14.5 63.9 926 | 8,06 To 205 14 63 92 |
| Savings Absolute Value Heat | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade | £M (NPV) £M (NPV) TWh pa £/MWh £M pa £M (NPV) | 0 0 To 2020 0.0 59.2 0 0 | 1,550 1,897 To 2030 7.1 62.8 443 947 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 | 8,06 To 205 14 63 92 8,71 |
| Savings Absolute Value Heat Absolute Value | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) | £M (NPV) £M (NPV) TWh pa £/MWh £M pa £M (NPV) kg/MWth | 0 0 0 70 2020 0.0 59.2 0 0 0 232 | 1,550 1,897 To 2030 7.1 62.8 443 947 228 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 228 | 8,06 To 205 14 63 92 8,71 22 |
| Savings Absolute Value Heat Absolute Value | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions | £M (NPV) £M (NPV) TWh pa £/MWh £M pa £M (NPV) kg/MWth 000 te pa | 0 0 0 70 2020 0.0 59.2 0 0 0 232 0 | 1,550 1,897 To 2030 7.1 62.8 443 947 228 1,611 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 228 3,306 | 8,06 To 205 14 63 92 8,71 22 3,30 |
| Savings Absolute Value Heat Absolute Value Fossil gas | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade | £M (NPV) £M (NPV) TWh pa £/MWh £M pa £M (NPV) kg/MWth | 0 0 0 70 2020 0.0 59.2 0 0 0 232 | 1,550 1,897 To 2030 7.1 62.8 443 947 228 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 228 | 8,06 To 205 14 63 92 8,71 22 3,30 |
| Savings Absolute Value Heat Absolute Value | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade | £M (NPV) £M (NPV) TWh pa £/MWh £M pa £M (NPV) kg/MWth 000 te pa 000 te | 0 0 0 0 0 0 0 0 232 0 0 0 0 0 | 1,550 1,897 To 2030 7.1 62.8 443 947 228 1,611 5,144 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 228 3,306 34,552 | 8,06 To 205 14 63 92 8,71 22 3,30 67,60 |
| Savings Absolute Value Heat Absolute Value Fossil gas | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced Executive decarbonisation decarbonis Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade Executive emissions by decade Executive emissions by decade Executive emissions by decade | £M (NPV) £M (NPV) TWh pa £/MWh £M pa £M (NPV) kg/MWth 000 te pa 000 te £/MWh | 0 0 0 0 0 0 0 0 232 0 0 0 0 139.2 | 1,550 1,897 To 2030 7.1 62.8 443 947 228 1,611 5,144 130.1 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 228 3,306 34,552 124.1 | 8,06 To 205 14 63 92 8,71 22 3,30 67,60 118 |
| Savings Absolute Value Heat Absolute Value Fossil gas | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) | £M (NPV) £M (NPV) TWh pa £/MWh £M pa £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M pa | 0 0 0 0 0 0 0 0 232 0 0 0 0 139.2 0 0 0 0 0 | 1,550 1,897 To 2030 7.1 62.8 443 947 228 1,611 5,144 130.1 1,120 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 228 3,306 34,552 124.1 1,803 | 8,06 To 205 14 63 92 8,71 22 3,30 67,60 118 1,72 |
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| Savings Savings Absolute Value Fossil gas Absolute Value Heat pumps Absolute Value | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) Cumulative Net Present Value by decade carbon intensity Annual Cost (inc reinforcement) Cumulative Net Present Value by decade carbon intensity Annual Cost (inc reinforcement) Cumulative Net Present Value by decade carbon intensity Annual emissions Cumulative emissions by decade es Levelised cost of heat | £M (NPV) £M (NPV) £M (NPV) TWh pa £/MWh £M pa £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M pa £M (NPV) kg/MWth 000 te pa 000 te £/MWh | 0 0 0 0 0 0 0 0 232 0 0 0 0 232 0 0 0 0 | 1,550 1,897 To 2030 7.1 62.8 443 947 228 1,611 5,144 130.1 1,120 2,670 29 204 67 40 7 113.1 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 228 3,306 34,552 124.1 1,803 11,847 15 214 3,502 109.9 | 8,06 To 209 14 63 92 8,71 22 3,30 67,60 1118 1,72 18,49 2 4,57 107 1,55 |
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| Savings Savings Absolute Value Fossil gas Absolute Value Heat pumps Absolute Value | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump Fes for GB at 10% (Method 2) Heat displaced Es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade Es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual Cost Cumulative Net Present Value by decade Es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative Net Present Value by decade Es Levelised cost of heat Annual Cost Cumulative emissions by decade Es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity | £M (NPV) £M (NPV) £M (NPV) £M (NPV) TWh pa £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth | 0 0 0 0 0 0 59.2 0 0 232 0 0 139.2 0 139.2 0 0 139.2 0 | 1,550 1,897 1,897 70 2030 7.1 62.8 443 947 228 1,611 5,144 7 228 1,611 1,120 2,670 29 204 67 29 204 67 113.1 798 1,815 30 | 7,210 6,025 To 2040 14.5 63.9 926 5,229 228 3,306 34,552 7 124.1 1,803 11,847 15 214 3,502 109.9 1,591 9,299 27 | 8,00 To 201 14 63 92 8,71 22 3,30 67,60 1118 1,72 18,49 2 4,55 100 1,55 15,22 2 3 3 2 3 3 2 3 3 3 3 3 3 3 3 3 3 3 3 3 |
| Savings Absolute Value Heat Fossil gas Absolute Value Heat pumps Absolute Value Heat pumps Absolute Value Hydrogen | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative emissions by decade Es Levelised cost of Heat (excl reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative emissions by decade Es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity Annual Cost Cumulative Net Present Value by decade Carbon intensity Annual emissions | £M (NPV) £M (NPV) £M (NPV) £M (NPV) £MWh £M (NPV) kg/MWh 000 te £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te pa £M (NPV) kg/MWth 000 te pa | 0 0 0 0 0 59.2 0 0 232 0 0 139.2 0 139.2 0 139.2 0 0 149.0 0 77 0 | 1,550 1,897 1,897 70 2030 7.1 62.8 443 947 228 1,611 5,144 7 228 1,611 5,144 7 30 2,670 29 204 67 7 113.1 798 1,815 30 215 | 7,210 6,025 To 2040 14.5 | 8,00 To 201 14 63 92 8,71 22 3,30 67,60 1118 1,72 18,49 2 4,55 100 1,55 15,22 2 3 3 2 3 3 2 3 3 3 3 3 3 3 3 3 3 3 3 3 |
| Savings Savings Absolute Value Heat Fossil gas Absolute Value Heat pumps Absolute Value Heat pumps Absolute Value Hydrogen Comparisons | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative emissions by decade Es Levelised cost of Heat (excl reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative emissions by decade Es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity Annual Cost Cumulative Net Present Value by decade Carbon intensity Annual emissions | £M (NPV) £M (NPV) £M (NPV) £M (NPV) £MWh £M (NPV) kg/MWh 000 te £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te pa £M (NPV) kg/MWth 000 te pa | 0 0 0 0 0 59.2 0 0 232 0 0 139.2 0 139.2 0 139.2 0 0 149.0 0 77 0 | 1,550 1,897 1,897 70 2030 7.1 62.8 443 947 228 1,611 5,144 7 228 1,611 5,144 7 30 2,670 29 204 67 7 113.1 798 1,815 30 215 | 7,210 6,025 To 2040 14.5 | 8,00 To 201 14 63 92 8,71 22 3,30 67,60 1118 1,72 18,49 2 4,57 107 1,55 15,22 2 32 7,97 |
| Savings Absolute Value Heat Fossil gas Absolute Value Heat pumps Absolute Value Heat pumps Absolute Value Hydrogen | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative emissions by decade es Levelised cost of heat Annual emissions Cumulative emissions by decade es Levelised cost of heat Annual cost Cumulative Net Present Value by decade Carbon intensity Annual Cost Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative emissions by decade | £M (NPV) £M (NPV) £M (NPV) £M (NPV) £MWh £M (NPV) kg/MWh 000 te £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M (NPV) kg/MWth 000 te pa | 0 0 0 0 0 0 59.2 0 0 232 0 0 139.2 0 139.2 0 0 139.2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 | 1,550 1,897 1,897 70 2030 7.1 62.8 443 947 228 1,611 5,144 1,611 5,144 1,611 1,120 2,670 29 204 67 29 204 67 113.1 798 1,815 30 215 787 | 7,210 6,025 To 2040 14.5 | 8,06 To 205 14 63 92 8,71 22 3,30 67,60 118 1,72 18,49 2 4,57 107 1,55 15,22 2 32 7,97 63,02 |
| Savings Savings Absolute Value Heat Fossil gas Absolute Value Heat pumps Absolute Value Hydrogen Comparisons Carbon | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative emissions by decade es Levelised cost of heat Annual emissions Cumulative emissions by decade es Levelised cost of heat Annual cost Cumulative Net Present Value by decade Carbon intensity Annual Cost Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative net Present Value by decade Carbon intensity Annual cost Cumulative net Present Value by decade Carbon intensity Annual emissions Cumulative net Present Value by decade Cumulative savings by heat pump relative to fossil gas Cumulative savings by hydrogen relative to fossil gas | £M (NPV) £M (NPV) £M (NPV) £M (NPV) TWh pa £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te 000 te pa 000 te 000 te 000 te 000 te | 0 0 0 0 0 59.2 0 0 232 0 0 139.2 0 139.2 0 139.2 0 0 139.2 0 | 1,550 1,897 1,897 70 2030 7.1 62.8 443 947 228 1,611 5,144 7 228 1,611 5,144 7 30 2,670 29 204 67 29 204 67 7 7 98 1,815 30 215 787 7 87 5,076 4,357 | 7,210 6,025 To 2040 14.5 | 8,06 To 205 14 63 92 8,71 22 3,30 67,60 1118 1,72 18,49 2 |
| Savings Savings Absolute Value Heat Fossil gas Absolute Value Heat pumps Absolute Value Heat pumps Absolute Value Hydrogen Comparisons | Cumulative decarbonisation by hydrogen relative to fossil gas Cumulative decarbonisation by hydrogen compared with heat pump es for GB at 10% (Method 2) Heat displaced es Levelised cost of heat Annual Cost Cumulative Net Present Value by decade Carbon intensity (delivered heat) Annual emissions Cumulative emissions by decade es Levelised cost of Heat (excl reinforcement) Annual Cost (inc reinforcement) Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual Cost (inc reinforcement) Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative emissions by decade es Levelised cost of heat Annual cost Cumulative Net Present Value by decade Carbon intensity Annual Cost Cumulative Net Present Value by decade Carbon intensity Annual Cost Cumulative Net Present Value by decade Carbon intensity Annual emissions Cumulative Net Present Value by decade Carbon intensity Annual Cost Cumulative Net Present Value by decade Cumulative emissions by decade Cumulative emissions by decade | £M (NPV) £M (NPV) £M (NPV) £M (NPV) TWh pa £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te £/MWh £M (NPV) kg/MWth 000 te pa 000 te pa 000 te pa 000 te 000 te | 0 To 2020 0 59.2 0 232 0 232 0 139.2 0 139.2 0 149.0 0 777 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 | 1,550 1,897 1,897 70 2030 7.1 62.8 443 947 228 1,611 5,144 7228 1,611 5,144 130.1 1,120 2,670 29 204 67 29 204 67 787 113.1 798 1,815 30 215 787 5,076 | 7,210 6,025 To 2040 14.5 | 8,00 To 201 14 63 92 8,71 22 3,30 67,60 1118 1,72 18,49 2 4,57 107 1,55 15,22 2 32 7,97 63,02 59,63 |

| Project code | NGGDGN03/1 | Question Number | 2 | |
|---|---|---|--------------------------------|--|
| Question date | 230816 (delivered 310816) | Answer date | 020916 | |
| Submission section question relates to | 3.3.1 | | | |
| Торіс | Benefits | | | |
| Question | The fall in the levelised cost of hydrogenetic estimate as shown in Table is itself in infancy. Can it be clarifie this source of hydrogen have been of benefits? | B4. In particular Bio d how the risks asso | -SNG which ciated with | |
| Notes on question | | | | |
| Answer The cost base for bio-hydrogen production is based on the work on the BioSNG project. In that project, costs of commercial scal were assessed in detail, for both early projects and `nth' of a kin demonstrated that this route could provide substitute natural ga parity with fossil gas over the course of the 2020's. | | | ale projects ind. This work | |
| | Production of hydrogen is a simpler process, requiring only a shift, rather than the full methanation of the syngas. Furthermore, the methanation catalysts are substantially more sensitive to impurities and so the upstream gas processing is also much simpler for hydrogen production. However, for the purposes of this assessment, the capital costs have not been reduced accordingly. Furthermore, for this application, the smaller scale and plant size has also been assumed. | | | |
| | Therefore, whilst it is plausible that hydroute at a similar cost on an energy bas hydrogen production used in this asses much higher. | sis to natural gas, the c | ost of | |
| | much higher. A further sensitivity analysis has been undertaken as shown in the table below. Increasing the cost of biohydrogen by a further 10% has the following impact on the benefits, reducing the 2050 NPV from £8,060m £7,287m for the 20% case and from £3,269m to £2,840m. | | | |

| | | Blend rate | To 2020 | To 2030 | To 2040 | To 2050 |
|-------------|--|--|-----------------------|--|--|-------------------------------------|
| | Cumulative NPV | (Method) | £million | £million | £million | £million |
| | | 20% Blend (M1) | 0 | 1,771 | 5,518 | 7,287 |
| | GB Values | 10% Blend (M2) | 0 | 785 | 2,267 | 2,840 |
| | Licensees Values | 20% Blend (M1) | 0 | 1,116 | 3,476 | 4,591 |
| | (63% of GB) | 10% Blend (M2) | 0 | 495 | 1,428 | 1,789 |
| | Post Trial | Either blend | 0 | 0.4 | 0.7 | 0.7 |
| | Were costs to inc solution and wou In summary, the through conserva that at this level alternative supply | ld play a greater risks associated ative initial figure the costs are the | vith bio-les, a sensi | elivering the hydrogen ha tivity asses | e hydrogen ave been a sment, and | required. ddressed I the fact |
| Attachments | | | | | | |

| Project code | NGGDGN03/1 | Question Number | 3 | |
|---|---|--|--|--|
| Question date | 230816 (delivered 310816) | Answer date | 020916 | |
| Submission section question relates to | 3.3.1 | | | |
| Торіс | Benefits | | | |
| Question | Can it be clarified how net benefits what assumptions are made about system wide costs would be incurre Dodds and Demoullin estimated con household). Could the levelised cos figures. | additional R&D costs ed (eg for full H2 dep nversion costs of £50 | , what loyment - 0 per | |
| Notes on question | | | | |
| Answer | The purpose of this project is to assess hydrogen blend which can be delivered without requirements for changes to co the network. | across the gas distribu | tion network | |
| | The figures cited from Dodds and Demo the conversion of their appliances, dete 100% hydrogen. These costs do not ex HyDeploy. | ectors and meters to op | erate on | |
| | The HyDeploy project is designed to provide the core R&D required to establish this route for decarbonisation. However, there are some addition development costs, which are acknowledged: | | | |
| | As laid out in the bid, it is expect network will be necessary prior be a lower cost project than this much of the core science and excollated in HyDeploy, but also be transferred to such a trial. Adoption of hydrogen as a blend methodologies. Alternative sour the existing Flow Weighted Aver hydrogen-blending is another fachange in this area. This work is the Future of Billing Methodologies. | to wider roll out. This is a first HyDeploy trial, bo vidence base will be dev ecause key equipment of d is likely to require cha ces of natural gas alrea rage CV approach needs ctor which supports the s already being address y NIC proposal. | expected to oth because reloped and can be nges to billing dy mean that s review; e need for sed through | |

| | The vast majority of the consumption will be for the provision of heat. However, it is recognised that there will also be CHP engines and similar small generators on the system. These will have different sensitivities to hydrogen blends compared with conventional heating demands. NGGD and NGN have already identified this, and are proposing to develop an NIA project to investigate it. It was decided that this should be separate from the NIC project due to the different nature of the investigation. However, this can be cost effectively hosted at the Keele site, using a CHP unit on the campus. It is expected that there is also a role for auxiliary R&D work, such as providing more cost effective gas analysis equipment for hydrogen – natural gas compositional measurements for injection sites. Whilst these R&D costs are in addition to HyDeploy, combined they are expected to be less than the cost of the current proposal. Therefore, against a decarbonisation route which has the potential to save £8billion, they would not substantially change the economic justification. |
|-------------|---|
| Attachments | |

| Project code | NGGDGN03/1 | Question Number | 4 |
|---|---|--|--|
| Question date | 230816 (delivered 310816) | Answer date | 020916 |
| Submission section question relates to | 3.3.1 | | |
| Торіс | Benefits | | |
| Question | Cost/carbon savings are based on is there a risk that 10% may not be testing etc. is conducted? "avoidance of network reinforceme included in cost savings. Should it reinforcement may be needed for r deployment i.e. electrification of ve | e achievable once app ent otherwise require not be acknowledge t easons other than he | bliance d″ is hat network |
| Notes on question | | | |
| Answer | This project builds on substantial work the UK and in Europe into the blending examples are: The Ameland Project in Holland 20% were injected. The HSE (2015) issued a literate 'concentrations of hydrogen in r unlikely to increase risk from wire appliances to consumers or mere In Germany parts of the network 10% hydrogen into the network 10% hydrogen 10% hydrogen | of hydrogen into gas no (2007-2011) where ble ure review which observa- methane of up to 20% b ithin the gas network or mbers of the public.' k are already permitted ugh the HyStart project blends in the UK contex a blend between 10-20 is a reasonable approact in innovation project, an etailed evidence base for le that the programme of blend level may not be | etworks. Key nds of up to yed that by volume are from gas to deliver have t and have % should not ch. d that the pr hydrogen could identify achievable. |

| | network, or very specific changes which could be required. In this case, part of the output of this project would be to recommend the appropriate route forward and a successful outcome could be below 10%. |
|-------------|---|
| | The level of network reinforcement required has been based on the level of capacity specifically required to deliver the number of heat pumps identified in the scenario. In this case a total reinforcement capacity of 8.8GWe for the 20% case with a discounted cost of \pounds 2,640m across transmission and distribution. |
| | Other assessments of widespread electrification of energy have substantially higher levels of assumed reinforcement capacity to accommodate greater levels of heat pumps as well as vehicle electrification etc (For example Delta ³ indicated a discounted cost of £12-20,000m of reinforcement costs for such a scenario). |
| | In reality partial reinforcement may be challenging given the potentially diverse geographical uptake of heat pumps. |
| | Therefore it is acknowledged that network reinforcement may be required for wider reasons, but the figures used here are conservative, particularly recognising that other costs, such as associated increases in generation capacity have not been included. |
| | References |
| | ¹ PILOT PROJECT ON HYDROGEN INJECTION IN NATURAL GAS ON ISLAND OF AMELAND IN THE NETHERLANDS, M.J. Kippers et al, International Gas Union Research Conference 2011 |
| | 2 Injecting Hydrogen into the gas network – a literature search' Hodges et al HSE (2015) |
| | ³ "2050 Pathways for Domestic Heat" Delta EE, October 2012 |
| Attachments | |
| | |

| Project code | NGGDGN03/1 | Question Number | 5 |
|---|--|-----------------------|--------|
| Question date | 250816 (delivered 310816) | Answer date | 020916 |
| Submission section question relates to | 2.3.3 | | |
| Торіс | General | | |
| Question | Does the 'accredited by Ofgem' referes the 'accredited by Ofgem' referes to what of the section 7 of your submitted of the section for the section fo | you are looking for a | |
| Notes on question | | | |
| Answer | ion | | |

| | project provides a site to test such equipment, although the development pathway is expected to be longer. |
|-------------|---|
| | |
| Attachments | |

| Project code | NGGDGN03/1 | Question Number | 6 |
|---|---|--|---|
| Question date | 250816 (delivered 310816) | Answer date | 020916 |
| Submission section question relates to | Section 7 | | |
| Торіс | General | | |
| Question | While we may have a view on the u does Ofgem have a formal role to a NGGD? | | |
| | Broadly, what does the process for timings be? | this look like and wh | at are the |
| Notes on question | | | |
| Answer | Yes, OFGEM will have a role in approvir regard to Calorific Value for the purpos | - , | NGGD with |
| | The Declared CV approach is one which is permitted by the Gas (Calculation of Thermal Energy) Regulations (part III). For example it is used within the Scottish Independent Undertakings. The network proposed for the HyDeploy project is a closed network with a single point of entry. | | |
| | As noted in the application, the vast majority of the gas supplied by Keele is consumed within its own buildings, therefore the volume of gas and number of customers affected is small, and so this is considered to be the most appropriate method to safeguard their interests. | | |
| | As part of the project, the team will develop the evidence base to submit to OFGEM, justifying the approach, and how it will ensure that the customers on the network are not disadvantaged. This will also include the proposed basis to set the CV, as well as how the CV will be periodically tested to demonstrate that the figure used is conservative in favour of the customers. | | e customers ne proposed cested to |
| | OFGEM will then review the evidence to networks the proposed CV must be adv three months prior to being implement communications plan it will be possible directly. | vertised in appropriate p ed. In this case, as part | oublications t of the |
| | Whilst the overall process may be time injection of hydrogen is not scheduled | - | |

| | of the project, and therefore it is not perceived as a major risk to the project programme. The project team will commence this process at the start of the project, and expects to be able to agree the approach with Ofgem by the end of the first phase (end of Q4 of the programme). |
|-------------|---|
| Attachments | |

| Project code | NGGDGN03/1 | Question Number | 7 |
|---|---|---|--------------------------------------|
| Question date | 090916 | Answer date | 150909 |
| Submission section question relates to | | | |
| Торіс | | | |
| Question | Please can you provide more inform issues that need to be addressed for used on the distribution network? chart/checklist including evidence differences if the NTS is used pleas | or hydrogen to safely This should be in the required by HSE. If t | blended and form of a here are |
| Notes on question | | | |
| Answer | Please see Attachment which shows in | fographic which answer | this question |
| Attachments | NGGD_HyDeploy_090916_Q7_Attachn | nent.pdf | |

Main issues that need to be addressed for hydrogen to safely blended and used on the Distribution Network

Scope of works as discussed with HSE:

Short Term Appliance Behaviour

Long Term Appliance Behaviour

Effect of Hydrogen on materials

Risk of poor mixing

Fire and Explosion risk

Hydrogen Detection

Desk based work

Sift all literature sources for relevance to Keele and present information for consideration by

Detailed design of lab based appliance testing and materials testing

Flame speed modelling to verify combustion properties of hydrogen /gas mixtures

HSE

Detailed design for mixing unit Review of emergency response plans

Baseline computer modelling Detailed specification of safety critical instrumentation for composition measurement and hydrogen detection **HAZOP** for injection system including

area classification

exercise

Laboratory testing Laboratory testing of 18 appliance types to determine safety performance Accelerated laboratory testing of 2-3 appliances to determine long term appliance performance

HYDEPLOY PROJECT

Tensile testing of component materials e.g. copper and solder when exposed to hydrogen

Integrity testing of fusion joints that have been exposed to hydrogen

Laboratory testing of composition analyser to verify functionality

Controlled hydrogen / gas releases to verify gas detection

methodologies

pipe) **Baseline integrity** survey of the network **Baseline materials** survey of the network Safety preparation work including changes to zoning / ventilation as required Recalibration of fixed site detection instruments Safe commissioning

Pre-trials work

all appliances to

check integrity of

installation /

performance

results

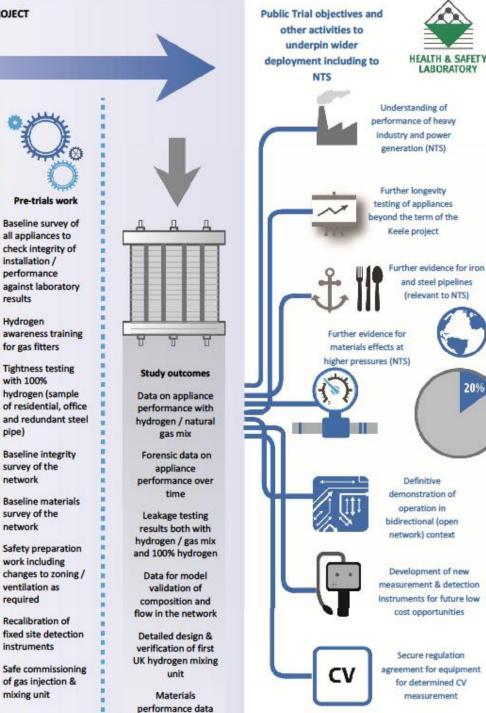
Hydrogen

for gas fitters

with 100%

Tightness testing

of gas injection & mixing unit



demonstration of operation in bidirectional (open network) context

Development of new measurement & detection instruments for future low cost opportunities

20%

HEALTH & SAFETY

LABORATORY



| Project code | NGGDGN03/1 | Question Number | 8 |
|---|---|---|--|
| Question date | 090916 | Answer date | 150916 |
| Submission section question relates to | | | |
| Торіс | | | |
| Question | "The cost of buying and installing a large sum of the cost of the project | - | makes up a |
| | (i) Why does hydrogen need to be onsite rather than shipped in? | produced by an electi | rolyser |
| | (ii) Could the electrolyser be renter could you provide the costs of rent to buying the electrolyser. Alternat hand? Is possible, please provide t electrolyser and it's expected lifeti | ing, if that is possible ively can it be purcha he cost of a second h | e, compared ased second |
| | (iii) Can you provide costings and r hydrogen brought and used from a compared to procuring and using a | safe place on the car | npus, |
| Notes on question | | | |
| Answer | (i) Why does hydrogen need to be proc than shipped in? | luced by an electrolyser | onsite rather |
| | Both approaches have the potential to required. However the university has a large inventories of pressurised hydrog project strategy proposed in the bid, w demand by the electrolyser. The attribu summarised in Table 1 overleaf, and a Section (iii) below, along with Table 2. | lways had safety concer en onsite. This has info here hydrogen is produ- utes of both approaches | rns about rmed the ced on are |
| | The volume of hydrogen required for the a pressurised hydrogen storage facility if it is not produced onsite. Given the lefor cost effective delivery of hydrogen, level rather than in university research requirement to minimise the potential is | to be built on the univer- evel of demand and the storage would be on an quantities. The Univers | ersity campus requirements industrial ity has a |

staff of such a facility and would have an obligation to ensure that risks are managed and appropriate procedures and policies are in place, compliant with necessary legislation. This would not be such an issue on an appropriately selected industrial site, but is viewed differently on a residential campus.

The project has been designed with the co-location of the hydrogen production unit and grid entry unit at the university energy centre at the heart of the campus with associated infrastructure. The electrolyser produces hydrogen at low rates (2.5g/s), with production stopped in under 1 second in emergency conditions, therefore inventories are extremely low. As discussed in Section (iii) below, cost-effective delivery and security of supply requires volumes of between 0.25 and 0.5 tonnes of hydrogen (the equivalent of over 500 conventional gas cylinders). Therefore such a solution would require that the hydrogen is stored away from existing facilities and dwellings at the edge of the campus. This entails additional cost for further pipeline infrastructure and implications of services and operation of the facility. Vehicle delivery must also be managed safely with appropriate gas manifolding and drive away protection and emergency shut down facilities.

The Keele site and the nature of its main access routes mean that additional lorry movements are a concern for the university and its community. It has previously rejected plans to convert one of the boiler houses on campus to biomass due to the need to have 2-3 lorry movements a week on campus. This is the same level that would be required over the winter for hydrogen deliveries. There are also some concerns about access in poor winter weather conditions.

With more infrastructure compared with an electrolyser solution, these costs are sunk and would require appropriate reinstatement following the project. Assuming that as planned, the Keele trial is followed by a trial on the public network, the electrolyser will be transferred, delivering enduring value from the asset through ongoing lower cost hydrogen production - a key benefit of this approach.

Electrolysis is one of the potential sources of hydrogen for blending in the future. Whilst not a core focus of the project, a supplementary benefit of the use of an electrolyser is to provide valuable long term operational data under real gas network load-following conditions.

In summary, the proposed project approach of using an electrolyser avoids key risks and offers a number of benefits. However, it is recognised that this needs to be assessed against the costs, which are shown in part (iii).

(ii) Could the electrolyser be rented rather than bought? Please could you provide the costs of renting, if that is possible, compared to buying the electrolyser. Alternatively can it be purchased second hand? Is possible, please provide the cost of a second hand electrolyser and it's expected lifetime.

The market for electrolysers of this scale for the production of hydrogen is not yet mature. Therefore no suppliers, including ITM, operate leasing business models for their products.

Similarly, there is not yet a second hand market for this type of electrolyser, with no evidence of suitable second hand products currently available for sale in the UK, Europe, US or Canada. Furthermore, the project team and Keele in particular would have strong reservations about safety and operability of such a unit. Having the operational support and commitment to process integrity from the Original Equipment Manufacturer is vital to deliver the project safely and to schedule.

However, as part of their commitment to the project, ITM have agreed to a buy-back option for the electrolyser; 50% before on-site commissioning, 25% post on-site commissioning. This non-standard commercial provision has been offered specifically for this project, which goes some way towards a rental model. This important provision has been included in the assessment below.

(*iii*) Can you provide costings and risk assessment of having hydrogen brought and used from a safe place on the campus, compared to procuring and using an electrolyser onsite.

The key attributes and risks of the two approaches are summarised in Table 1 below, and the costs compared in Table 2. Both the risks and costs are supported by the narrative below. In summary this shows that whilst there are some cost savings to be made for the trial at Keele through buying hydrogen and storing onsite, these are relatively limited, particularly when reviewed against the increased project risk profile. Assuming that as planned, the Keele trial is followed by a trial on the public network, the electrolyser will be transferred to continue to deliver further lower cost hydrogen.

Risks

A pressurised hydrogen storage facility on the Keele University campus site would have to comply with current legislation, and the University would have to show that it had met its duty of care obligations with appropriate safety cases developed.

Within the UK, the current legislation associated with the storage and handling of large volumes of dangerous materials are covered by the Control of Major Accident Hazards (COMAH) Regulations 2015. The regulation seeks to allow the identification of sites for major hazard, ensure control measures are in place to prevent major accidents and mitigation measured are in place to limit the effects of accidents. Whilst the volumes of gas expected to be stored would fall below the requirements for formal compliance under COMAH, the quantities are sufficiently material that the University would be seeking to ensure that its policies and procedures follow best practice and guidelines set out under these regulations.

Subject to confirmation of storage requirements based on efforts to minimise footprint and delivery frequency by tube trailer, planning permission would have to be sought and the local planning authority could impose limits on the capacity of the facility and make it a requirement to prepare accident prevention policies to address major accident hazards and for the protection of people and the environment which must be made available to contractors and employees at the site. In addition hazardous substances consent would be required.

Specific risk attributes of storage as compared with the electrolysis approach are shown in Table 1.

Basis for the costing comparison

<u>Campus siting</u>: To seek to address concerns regarding a large inventory of pressurised stored hydrogen, sites have been identified towards the edge of the Keele University campus, as shown in Figure 1 overleaf. Currently the most appropriate site is considered to be Plot 12 with sufficient available area (although the University is considering utilising an existing test well on part of this site for research / geothermal energy production, which could present a project risk). Note that building work is already under way on adjacent plots.

<u>Pipeline configuration</u>: The project has been designed with the co-location of the hydrogen production unit and grid entry unit at the university energy centre at the heart of the campus with associated infrastructure. Two revised configurations with storage were considered:

- (a) Location of just the hydrogen storage facility at Plot 12, with a dedicated hydrogen pipeline to the grid entry unit located at the Horwood Energy centre as before. Whilst this solution is least disruptive and shorter (900m), the minimum pipeline methodology recommended by the British Compressed Gases Association (BCGA), and required by current hydrogen users such as Shell is for seamless stainless pipelines in concrete ducting. Combined, the lay cost of this approach is over ten times more expensive per metre than conventional gas piping.
- (b) Location of both the hydrogen storage facility and grid entry unit at plot 12. This requires a longer pipe run (1600m length) as it requires an additional natural gas pipeline from the university to plot 12 and then the blended pipeline from Plot 12 to the existing G3 meter. However, this is consistent with the wider project, using conventional PE pipelines and lay methods and so substantially cheaper, even after accounting for the additional services required at the remote site. For the assessment here, this approach is assumed.

<u>Storage type:</u> three types of storage were considered; Multi Cylinder Packs (MCPs), trailers and dedicated storage. Hydrogen delivered by MCPs costs around 10 times that by trailer and for winter usage would require changeover every two hours at 20% blend. Trailers hold between 225-500 kg of storage depending on pressure (typically 200-350 barg) and length between 5.8-11.6m plus tractor unit. Purchase costs are between £180,000-£670,000 each depending on type and pressure, with dedicated storage solutions having similar characteristics. However, 200 barg trailers holding 225kg of usable gas (requiring changeover 2-3 times per week during the winter at 20% blend) can be hired from the major gases companies, offering

| | the most competitive solution for this application, and form the basis of the cost assessment. In all cases, decanting facilities including drive away protection, pressure reduction, gas distribution manifolding, emergency shut down facilities are required on site. |
|-------------|---|
| | <u>Costing data</u> : Where possible figures for comparison have been secured from suppliers such as the major gases companies, which are based on established supplier customer relationships, and estimates based on data developed in the initial bid. Assumptions have been included in Table 2. |
| | The assessment of costs includes only the direct costs applicable to the solution. It does not factor in the costs associated with managing the additional risks associated with the storage route. For example, it is clear that the management at Keele University has reservations about such an inventory of gas on its site, and so it is expected that there will be additional costs incurred to develop and present the safety case to their satisfaction. |
| | The costs are shown for the initial trial and Keele University only. The electrolyser asset is readily transferable, unlike the sunk infrastructure costs associated with storage. The expectation is that the hydrogen production equipment will be transferred to a follow on trial on a public network. Use of this asset allows continued lower cost hydrogen delivery, particularly where sited to exploit opportunities for lower cost electricity. |
| | Summary: As shown in Table 2, there are some cost savings to be made for the trial at Keele using the delivery and storage solution. However, these savings, of the order of £90,000, are relatively limited particularly when reviewed against the increased project risk profile discussed above and shown in Table 1. Assuming that as planned, the Keele trial is followed by a trial on the public network, the electrolyser will be transferred to continue to deliver further lower cost hydrogen, expected to more than offset the storage savings |
| Attachments | See 2 Tables and 1 Figure below |

| Attribute | Electrolyser | Storage | Implications |
|--|---|---|---|
| Campus location | Located at the energy centre with good access to all services | Located at the edge of the campus with additional pipeline and services connections required. | Project Cost |
| Site availability | Site already secured for project as part of development to date Identified site have potential competing uses, which represent a project delivery risk | | Project delivery risk |
| Site & infrastructure | Existing developed area with hard standing | Greenfield development | Project Cost |
| Foot print | One Iso Container, integrated into existing GEU footprint | Min 3 x footprint for storage plus necessary turning circle allowance for HGV delivery | Project Cost |
| Gas pressures | Gas delivery pressure at 2 barg to match the gas network | Storage at 200 barg | Safety risk requiring management |
| Potential hydrogen release volumes | With response times under 1s, and production rate of 2.5g/s, therefore limited | Storage inventory in excess of 225kg ; would require appropriate protection measures | Safety risk requiring management |
| Opportunity for release | Short, single and permanent pipeline to the grid entry unit Multiple and longer length pipelines | | Safety risk requiring management |
| Connections | Single iso container with 3 connections directly to the grid entry unit Multiple manifolding, requiring safe drive away connections etc | | Project Cost and Safety risk |
| Continuity of supply | of Only relies on continuity of electricity supply, which is good. Subject to maintain HGV trans access during the winter at performed and the supply of electricity supply which is good. Subject to maintain HGV trans access during the winter at performed and the supply of electricity supply which is good. Subject to maintain HGV trans access during the winter at performed and the supply of electricity supply which is good. Subject to maintain HGV trans access during the winter at performed and the supply of electricity demand. In extremis the road a supply which is good. | | Project disruption / data quality |
| Delivery requirements | very Once equipment delivered non- Regular HGV deliveries 2-3 per week. Campus rejected a biomass boiler | | Project Delivery risk |
| Project programme | Whilst the electrolyser procurement forms a substantial part of the phase 2 schedule, the Grid Entry Unit lead time is the same length, 'gating' the programme | Delivered hydrogen avoids the build time for the electrolyser, but the benefit cannot be realised. | No impact |
| Follow on project | trial, substantially reducing reduce | | Cost implications for follow on trial |
| Additional attributes, learning opportunities | Ability to secure evidence of electrolyser performance when load following gas demand under long term operational conditions | Some learning regarding storage, but considered to be BAU for appropriately selected sites in the future | Missed opportunity |

 Table 1: Attributes of Electrolyser and Delivery and Storage Solutions

| Base Case Electrolyser | | Delivered Hydrogen & Storage Comparison | | | |
|-------------------------------|----------|--|------------------------------------|---------|--|
| Fixed Costs | £ | Comment | Fixed Costs | £ | Comments |
| Electolyser Equipment costs | 676,962 | Taken from bid | Trailer unloading manifolds etc | 75,000 | Equipment Estimate provided by Gas supplier (trailers assumed to be hired as variable cost, below) |
| Factory Acceptance testing | 36,120 | Taken from bid, electrolyser only | Civil costs for site | 115,000 | Additional costs for larger site to accommodate two trailers plus HGV movements and greenfield site. Costs estimated based on initial project figures |
| Installation | 15,881 | Taken from bid, electrolyser only | Local control room | 6,000 | Orginally using Horwood Energy Centre. Assumes Portacabin Hire and installation |
| Commissioning | 53,631 | Taken from bid, electrolyser only | Communications | 12,000 | Provision for secure IT services to control room (formerly integrated into Energy Centre) |
| | | | Additional pipelines | 208,000 | Additional pipeline from university natural gas offtake to Plot 12, and return line for blended gas back to G3 meter (total additional length of approx 1600m compared with base case). Based on PE pipeline lay costs of £13,000/100m. |
| Total | 782,594 | | TOTAL | 416,000 | |
| Variable cost of hydrogen | 123,120 | Based on 20 tonnes per annum and Keele's prevailing electricity cost. | Variable cost of hydrogen | 203,000 | Based on 20 tonnes per annum. Data provided by Gas supplier. Trailer usable capacity of 225kg. Driver charge of £55/hr, Mileage at £1.15/mile, Call out of £80/delivery and based hydrogen at £50/HCM. Equates to £7150/te delivered cost plus hire charges for trailers (£5000/month) for 12 month period |
| Buyback provision | -195,000 | 25% as provided by ITM | | | Not Applicable |
| Net project costs | 710,714 | | | 619,000 | |
| Net saving using storage | | | | 91,714 | Keele trial only; expected to be more than offset in public trial |

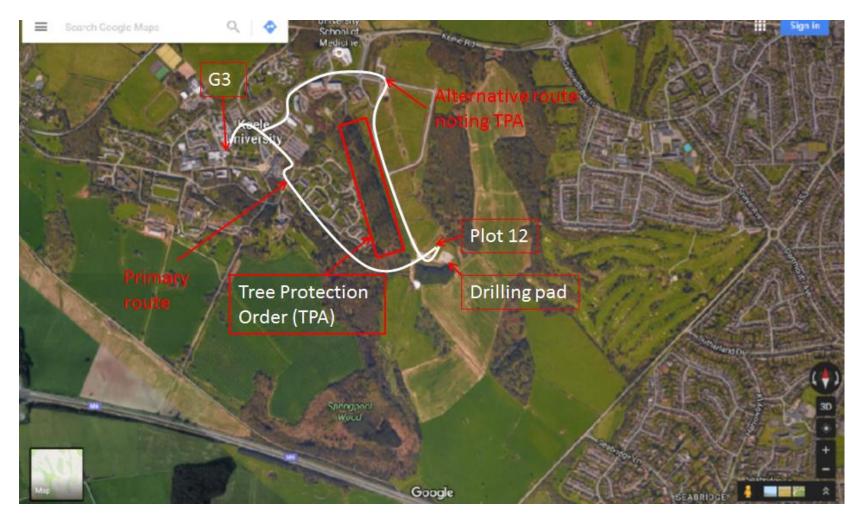


Figure 1 Site locations and routing

| Project code | NGGDGN03/1 | Question Number | 9 |
|---|---|--|---|
| Question date | 090916 | Answer date | 150916 |
| Submission section question relates to | 8 | | |
| Торіс | Customer Engagement Plan | | |
| Question | (i) Please can you provide a high le that will be used for customers one Oban? | | - |
| | (ii) Please can you include as an ex consolidation of work and learning future trails of hydrogen on the pu | on customer engage | - |
| Notes on question | | | |
| Answer | (i) As set out in Section 8 of the HyDeploy Bid document and in line with NIC Governance requirements, the final Customer Engagement Plan will have a structure and content which draws on the knowledge and experience acquired from similar previous engagement with customers, notably in the SGN Oban project. It is anticipated the Engagement Plan will be set out with a structure as indicated in the Overview below. | | |
| | The HyDeploy project is aware of the in customer engagement. At its heart is of addressing climate change and the carl consume, as well as how this solution p the UK consumer. In addition to inform and the integrity of the project structure the fact that we are doing something w customers will have concerns about ris lives. So there is a need to communica majoring on the fact that hydrogen has on the quality of the project planning a the fact that nothing will be taking place Whilst the immediate focus of the HyDe | communicating the impo- bon implications of the l provides a non-disruptiv- ning the customers abou- re, the strategy must al- which is new and so, bec- k and impact on their da- te effectively and sensit s been used in the UK bo- and the team, particular ce without the HSE's agr | vertance of heat we re solution for the benefits so recognise cause of this, ay-to-day cively, efore, focusing by HSL, and reement. |
| | Whilst the immediate focus of the HyDo and customers, it is also important to r engagement undertaken has wider imp customers are handled and the effectiv learning for the anticipated further roll | ecognise that the custo dications for the future a reness of the process wi | mer and the way II be essential |

includes the learning and benefits from the NG staff we will be training, and the appliance / boiler manufactures with whom we engage.

(ii) The learning about the communications plan will be included in the Public trial development; we will make this an explicit part of the SDRC 9.9, viz "Completion of definition of follow on network trial, including application of learning from the Keele customer engagement plan".

HyDeploy Customer Engagement Plan Overview

Executive Summary

1. Introduction

- This will explain the project background against the backdrop of climate change targets and heat decarbonisation, including the specific opportunities afforded by the Keele site.
- The requirement for an engagement plan will be explained and its structure will apply learning from various relevant sources e.g. the Oban project.
- The project's commitment to customers, notably Priority Services Customers, in terms of service continuity, safety and commercial integrity will be set out and this will be reflected throughout the Plan.
- Plan to be signed off by both OFGEM and Keele Ethics Committee before any customer engagement takes place

2. Proposed interactions with customers

This will cover the proposed set of communications and the customer experience, including:

- Initial customer contact and engagement e.g. initial information meetings, leaflets, information line
- Appliance testing and replacement: what the customer can expect on the day and the support that will be given in terms of making convenient appointments and after-care
- Continuing monitoring during field trial
- Continuing customer support for problems or concerns
- Close-out event to thank customers and present results

Further details about the methods and content will be given in the Communications Strategy below.

3. Audience

• The key audience is our Keele customers, both domestic and departmental which are the equivalent of a small town with the

| | following makeup: |
|----------------|--|
| | 67 Academic and Science Park buildings |
| | 152 student residential buildings |
| | 101 staff flats and houses – 47 owned by Keele and rented, 54 owner-occupied |
| • | The project starts with a key advantage of Keele University having a close relationship and knowledge of each of the properties included in the test site. Hence the target audience is well researched and segmented already. |
| • | The project will address anticipated customer expectations and also take into account customer feedback |
| 4. Co | mmunications strategy |
| | ommunication strategy will be comprehensive and use various media ieve the goals: |
| • | Core messages to key target audiences of what, when, why and how. |
| chang Newca | vill draw upon known public perceptions of gas appliances, climate e and, in particular, hydrogen using work such as the proposed NGN & astle University NIA on <i>Hydrogen in Everyday Energy Use: Perceptions,</i> ces and Possibilities. |
| • | Desired outcome and outputs will be set out clearly in line with the project plan. |
| • | Channels for engagement: meetings, drop-in sessions, household and general leaflets, website, social media, customer care line etc. |
| • | Branding of the project to establish a clear identity with customers and stakeholders involved in the project. |
| • | Communications phasing through the project; initial focus on awareness and answering concept and start-up questions (what, why, when, how), followed by regular update and feedback focus. |
| • | Communications framework map to ensure all communications are well integrated and also in line with Keele University communications standards. |
| • | Notifying Customers – covering formal notifications. |
| 5. Saf | ety information |
| • | Our safety culture: Safety is paramount in everything we are proposing to do at Keele and all project operations are to be approved by The Health and Safety Executive and Keele University. |
| • | The project team consists of world-leading organisations in the field of safety including as the Health and Safety Laboratories and Kiwa |

| | GasTech. |
|-------------|---|
| | Customer assistance: "don't walk by" if notice unexpected issues or are concerned about any aspect of safety. |
| | Risks: risk register, particularly customer-facing issues |
| | Unsafe situations procedure |
| | • Data Protection: identification and procedures (see below) |
| | 6. Customer consent |
| | Because of the nature of the site and the type of people affected, the issue of customer consent may be more straightforward than in a public setting. However, this does not mean the topic is taken lightly and this section will set out the approach to: |
| | Obtaining and documenting customer consent |
| | Customer participation |
| | 7. Data Protection Strategy |
| | Keele University already has a relationship with all the customers on site and an existing data Protection Strategy. This will form the basis of the project DP strategy to be agreed with OFGEM and the Keele Ethics Committee. It will deal with issues such as: |
| | • What personal data will we collect for the purposes of the project? |
| | How will personal data we collect be used? |
| | Who will we share personal data with? |
| | • How will consent for use of the personal data be obtained? |
| | Who owns the personal data? |
| | How will data or analysis be published? |
| | • How will we ensure we store and manage personal data securely? |
| | Compliance with NG and Keele standards and policies |
| Attachments | |

| Project code | NGGDGN03/1 | Question Number | 10 |
|---|--|---|---|
| Question date | 090916 | Answer date | 150909 |
| Submission section question relates to | | | |
| Торіс | | | |
| Question | Part of the project plan identifies the inspected. | hat a 6″ steel pipe mu | ıst be |
| | (i) Why does this pipe need to be in be needed if the project doesn't go | - | inspection |
| | (ii) What is the mitigation if repair these costs included in the project vs new asset life should Keele mak | cost? Given its depre | ciated cost |
| Notes on question | | | |
| Answer | The questions are briefly answered, the | en amplified in the narra | ative below. |
| | (i) To clarify, the pipeline is routinely in what has been identified and costed is <i>replacement</i> in order to risk manage exemptance the data provided, as described | the fact that the pipelin vecution of the project a | e requires |
| | (ii) The mitigation already identified is well as configuring and setting up the o testing. These costs have already been basis that this asset is not due for repla the requirements to set it up for dedica project. However, it is recognised that to the university, and so it is agreed th of the new pipeline itself is not borne b budget by £25,000. | old pipeline element for included in the project acement under business ated testing are inherent this will provide addition at it is appropriate that | dedicated budget on the as usual and t to the nal asset life the full cost |
| | An element of leakage is present throu transporters are obliged to undertake r register of elements of the network wh and this section of pipeline falls into thi | egular monitoring. Keel ich require particular ob | e maintains a |
| | Currently the agreed Safety Case for the operation indicates a residual asset life | | ess as usual |

| | However, in light of performance to date and in discussion with NGGD, NGN and the HSE it has been recognised that this element of the network would represent an uncertainty under hydrogen operation which would need to be factored into the Quantitative Risk Assessment. This uncertainty could adversely affect the QRA outcome. |
|-------------|---|
| | Given the wide range of factors which will need to be addressed for the first time in this project, it was agreed that to risk manage overall project delivery of the programme, this risk should be addressed such that it doesn't 'gate' the outcome for the wider network trial. |
| | However, this asset also provides a unique opportunity to undertake more dedicated and focused tests on this part of the network, including the existing transition from plastic to steel pipeline. This is particularly instructive as this is an old, in situ pipeline, with very limited experimental data available for such infrastructure. Furthermore BEIS identified that this provides a unique opportunity to undertake tightness testing with 100% hydrogen. |
| | It was therefore decided that this pipeline spur would be disconnected from the network, and the residual consumers at the end of this spur connected directly to Keele's G1 network. The existing pipeline asset will be disconnected, decommissioned, and reconfigured for direct connection to a dedicated supply and subsequent testing. |
| | The project budget is £80,000 for this work including £50,000 for the new pipeline itself. Although none of this work would be required at this stage if it weren't for the project, in recognition of the fact that it will deliver an element of asset life extension to Keele, it is agreed that only 50% of pipeline cost itself would be attributed to the project, reducing the overall budget by £25,000. |
| Attachments | |

| Project code | NGGDGN03/1 | Question Number | 11 | | |
|---|--|-----------------|--------|--|--|
| Question date | 090916 | Answer date | 150909 | | |
| Submission section question relates to | | | | | |
| Торіс | | | | | |
| Question | Please can you provide more detail on: (i) The business case for biohydrogen as source (ii) The long-term cost of the production of biohydrogen compared to the cost of natural gas, given learnings over the last year and also allowing for different scenarios for gate fees. | | | | |
| Notes on question | | | | | |
| Answer | (i) Business case for biohydrogen as source The business case for bio-hydrogen builds on the case for the production of BioSNG. This has been developed and refined over the last 3 years providing the basis for the award of NIC funding under previous rounds of the competition. Key elements in the business case are: Strategic: The delivery of low carbon gas to deliver non-disruptive heat to consumers using the UK's existing gas distribution asset and customers' existing heating systems. Feedstock: Sufficient feedstock identified to deliver 100TWh per annum on a full potential basis by 2050. Sufficient waste is currently being exported deliver nearly 10TWh pa alone with nearly 4 times that currently being landfilled. Technology: the production of a high quality syngas from waste derived material which is converted through the water gas shift and catalytic methanation to a fungible fuel. Being piloted with a commercially operating demonstration project underway and the first large scale plant planned for 2020/21. Similar pure biomass project operating and delivering gas to the grid in Sweden. An overall cost base from waste feedstocks which has the prospect of being cost competitive with conventional fossil fuels. Existing support structures, particularly the RHI which explicitly support injection of biomethane into the grid to support the transition to that point. | | | | |

The numbers supporting the business case have been refined through the work of both NGGDGN01 and NGGDN02 as described below. The business case for hydrogen is very similar, but with the following key differences: The process is substantially simplified. The most sensitive and complex catalytic reaction is the methanation stage which is no longer required, and the upstream gas polishing can also be simplified as shown schematically below (Full green processes remain, lighter green process simplified and light green processes removed). This both reduces capital cost and increases process resilience. DRY & GAS COMPR. GASIFY **PLASMA** WET POLISH SCRUB METH CO₂ WGS (H2 METH CAPT. POLISH Hydrogen has the potential to be more valuable than natural gas (as typically hydrogen is produced by processing natural gas), enabled by the development of wider markets such as fuel cells and vehicles. Longer term this provides valuable additional markets to drive the development of bio-hydrogen production. (ii) The long-term cost of the production of biohydrogen compared to the cost of natural gas, given learnings over the last year and also allowing for different scenarios for gate fees. The long term cost of production has been based on the work from NGGDGN01 and NGGDN02. This has informed: (a) Process performance: Operation of the pilot plant has confirmed the thermodynamic and kinetic modelling of the process, underpinning the performance assumptions made, including greenhouse gas emissions.

(b) Capital costs: The overall costs of construction have remained broadly in line with those anticipated at the start of the project. The demonstration project has required the team to go to market for firm pricing. Other than the specific addition of CO_2 liquefaction process in order to demonstrate utilisation of CO_2 (such CO_2 savings have not been assumed here) there has been a 3.5% increase on the overall costs, primarily due to movements in the pound since Brexit.

| | (c) Operational and gate fee assumptions: Figures for operational costs have been refined, with minor changes. There have been no changes to feedstock assumptions, with waste for the demo project at £65/te. Gatefees payable for RDF have risen from £72.50 +/- £7.50 to £85 +/-£5 between June 2014 to June 2016 (Lets Recycle). This is driven in part because landfill tax has now increased to £84.40/te such that total landfill costs are £100-£110/te. Export of RDF is expected to approach 4 million tonnes over the next year. | | | | | | |
|-------------|---|---|------------|----------|-----------|--------------|----------|
| | £35/MWh f | ojections for FO for a 315GWh p to 2030, recogr | lant or £2 | 1/MWh fo | or a 665G | Wh larger pl | ant over |
| | | g the financial ve figures have | | | drogen pr | oduction, | |
| | Capital and operational costs for production have been maintained at the BioSNG levels, despite the process simplification described above. Beyond 2030, it has been assumed that costs fall at 0.5% per annum through incremental learning Only the smaller scale of plant has been assumed. Gatefees have been set substantially lower Additional costs for hydrogen storage and connection to the grid have been included. | | | | | | |
| | These figures are provided in the set of assumptions in Appendix B.4 (p57) of the Hydeploy bid with hydrogen levelised costs shown in the table below. | | | | | | |
| | These are conservative figures, but a sensitivity analyses to capex and gate fee shows that whilst the bio hydrogen uncertainty has an impact on the overall savings (using the 20% blending case as an example, as per the 2050 column of table B.3.1), it does not fundamentally change the merit of hydrogen blending. In reality it would probably lead to different mixes of hydrogen sources. | | | | | | |
| | | Bio-hydrogen | FOAK | 2030 | 2050 | NPV saving | |
| | | sensitivities | £/MWhr | | | £M cum. | |
| | | Baseline | 77 | 52 | 46 | 8060 | |
| | | Capex +20% | 86 | 58 | 51 | 7190 | |
| | | Capex -20% | 67 | 46 | 41 | 8930 | |
| | | Gatefee £22.50 | 83 | 59 | | | |
| | | Gatefee £52.50 | 70 | 45 | 40 | 9078 | |
| Attachments | | | | | | | |

| Project code | NGGDGN03/1 | Question Number | 12 | |
|---|--|---|--|--|
| Question date | 26-09-16 | Answer date | 04-10-16 | |
| Submission section question relates to | | | | |
| Торіс | | | | |
| Question | Can you compare the use of hydrog in relation to other future energy so to district heating from municipal v economic case for hydrogen to futu | cenarios. For example vaste? How sensitive | e, compared | |
| Notes on question | | | | |
| Answer | meeting on 30/09/16 shown below. Various commentators have projected a (six pathways to 2050 have been consi and Climate Change (DECC), the Commenergy Technologies Institute (ETI), Na Centre (UKERC) and Delta EE). Commenert challenge is sufficiently large and solution. The most recent assessment by the Pol September 2016) recognises that succe requires solutions which are readily add scenarios which place great weight on the district heating, they put forward a more solution. | Various commentators have projected a range of future energy scenarios (six pathways to 2050 have been considered by the Department of Energy and Climate Change (DECC), the Committee on Climate Change (CCC), the Energy Technologies Institute (ETI), National Grid, the UK Energy Research Centre (UKERC) and Delta EE). Common to all is the fact that the size of the heat challenge is sufficiently large and diverse that there is no single solution. The most recent assessment by the Policy Exchange ('Too hot to handle' September 2016) recognises that successfully delivering low carbon heat requires solutions which are readily adoptable by customers. Compared with scenarios which place great weight on the adoption of heat pumps and | | |
| | building efficiency, (b) improving gas a carbon/renewable gas delivery, (d) add pumps, and district heating). District heating undoubtedly has a role Exchange report outlines that 1% of UP via district heating with a realistic futur energy in its recent report shows that i population density, but even high uptal | to play in the mix. The k households are current re potential of 10-15%. t is a good solution for a | Policy Policy tly supplied Element areas of high | |

| heat zones. Element energy suggests that EfW could contribute 3TWh to district heat demand. Hydrogen blending as shown by the HyDeploy work could provide up to 29TWh; against the Carbon Plan requirement of over 83TWh low carbon heat by 2030 it is clear that all solutions are required. 3TWh of waste derived heat would require 1-2 million tonnes of waste per annum depending on how the heat is delivered. Against current landfill and export levels equating to 17 million tonnes, this does not substantially affect the availability of waste for the proposed volumes of hydrogen from this source. Work by Poyry assessed the costs of heat delivered by district heating. The figures they determined for baseline gas generation, and heat pumps were broadly consistent with the figures given in the HyDeploy assessment £60 and £130/MWh respectively, compared with hydrogen at £107/MWh. Their view of DH with EfW was in excess of £200/MWh. The exact cost does depend on assumptions made about EfW, and in reality the figure may be somewhat lower than this. However, they assess conventional gas CHP solutions with DH at around £110/MWh, which is not a 'low carbon' solution, rather a more efficient use of gas; CO2 is still emitted. In this context, decarbonised hydrogen has a valuable and important role, particularly since it could also have a role in district heating sche | | |
|--|-------------|--|
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| Attachments | | carbon savings, but in parallel with solutions such as low carbon gas delivery which is non-disruptive for the customer and which valorises existing |
| Attachments | | |
| | Attachments | |



- · Sets out a customer focused framework recognising the strategic role for gas, in light of over 80% of households being heated by gas
- Heat pumps & district heating are core 'Alternative Technologies'

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Policy Exchange 09/16

solution





Q1: Heat Networks & Energy from Waste

- Currently: 1% of UK households, Future: 10-15% (Too Hot to Handle)
- Good for populations of high density, but even high uptake covers <10% of UK 1km² heat zones
- Opportunity to deliver 3TWh pa of heat from EfW facilities via district heating systems (Element Energy)
- Challenges to overcome
- Capital cost of networks
 Disruption of networks

 Disruption in households Customer choice
 New build estates need policy intervention

 Annual heat demand in benign climate

 Continuity of waste processing Forfeited power (EFW plant) Counterparty risk

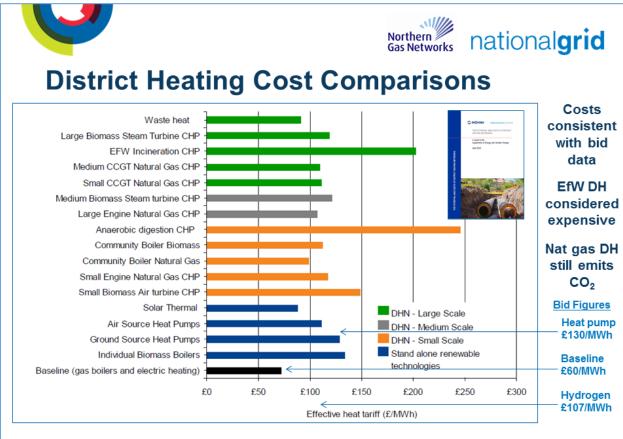


Plymouth EfW CHP January 2016

Under an energy services agreement with the Ministry of Defence, MVV Devonport will supply 24MW of electricity and steam to the adjacent Naval Dockyard, the largest naval base in Western Europe. Paul Carey, managing director of MVV Environment Devonport, said plans to develop a local district heating scheme for residents living close to the site were again "under review". The strategy was previously thought to have been scrapped, following a feasibility study with Plymouth city council which found the size of the heating scheme would make it impracticable

Heat Networks have a role, but alongside existing infrastructure solutions

3



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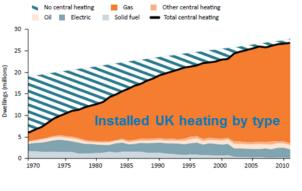
Potential and costs of district heating networks', Poyry, Aecom, Faber Maunsell (2009)





Q1: How sensitive is the economic case for hydrogen to future market changes?

- Fundamental costs of decarbonisation by hydrogen are not changed even with elements of heat pumps and district heating networks
- Some impact on *level* of contribution if gas demand reduces further, noting other solutions still likely to include elements of gas consumption
- · Using existing gas infrastructure is the most customer focused solution
- Barriers to deployment far lower than solution requiring new infrastructure



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5

| Project code | NGGDGN03/1 | Question Number | 13 | |
|---|--|---|---|--|
| Question date | 26-09-16 | Answer date | 04-10-16 | |
| Submission section question relates to | | | | |
| Торіс | | | | |
| Question | If the project is successfully comple Can you provide a bit more detail o network trial? | | - | |
| Notes on question | | | | |
| Answer | The following is a commentary supporting the slides used in the bilateral meeting on 30/09/16 shown below. The HyDeploy project is the first UK deployment of a hydrogen – natural gas blend onto the distribution network. As described in the bid, and supported by experts such as the HSE and DNV-GL, this first trial will be on a closed, private network in order to risk manage project delivery and potentially enable more ambitious levels of blend that would otherwise be achievable than executing the first trial on a public network. | | | |
| | However, a public network trial as alwa next step towards widespread deploym safety case and application for exempti build on the wide ranging foundational Keele, as shown in the Infographic devi- will also draw on wider parallel work in users such as CHP facilities. Ideally tha related to revised billing methodologies measurement equipment. (Whilst a pub- approaches as proposed at Keele, it wo more enduring strategies, representative | ent. The customer enga on for that public netwo work from the HyDeplo eloped in response to q the industry relating to t public trial will also bu and OFGEM 'Directed' plic trial could use the s ould be strongly preferal we of future deployment | agement plan, ork trial will y project at uestion 7. It other gas uild on work compositional ame ole to execute | |
| | It is expected that this public trial will s through the same model as the Keele p exemption for anaerobic digestion plan | project. However, as wit | h the oxygen | |

'class exemption' and ideally enduring regulatory changes.

The detailed public trial will be defined as part of the HyDeploy programme (Work Package 14). This includes a scientific gap analysis undertaken at that point in the project. However, the key aspects are detailed below

Site Selection: the site will be selected to be statistically representative of the GB distribution network. This will be undertaken building on the methodologies used in the opening up the gas networks project. It will be an 'open' network, accommodating gas flowing in from various sources, with the implications this will have for varying hydrogen blend compositions over time. Suitability for locating the hydrogen production and injection facilities will also be an important criterion. NGN and NGGD have already undertaken some early feasibility assessments of a potential site, in particular to model the flows of hydrogen in an open network under a variety of conditions. It also meets the criteria for local stakeholder support regarding location of production and injection equipment. However, this site will be evaluated alongside other sites, particularly with regard to statistical representativeness of the GB network.

Equipment: The production and injection facilities will be re-used, as well as monitoring equipment. However, it is anticipated that the public trial would provide the opportunity to deploy OFGEM Directed Composition measurement equipment, rather than relying on a declared CV basis.

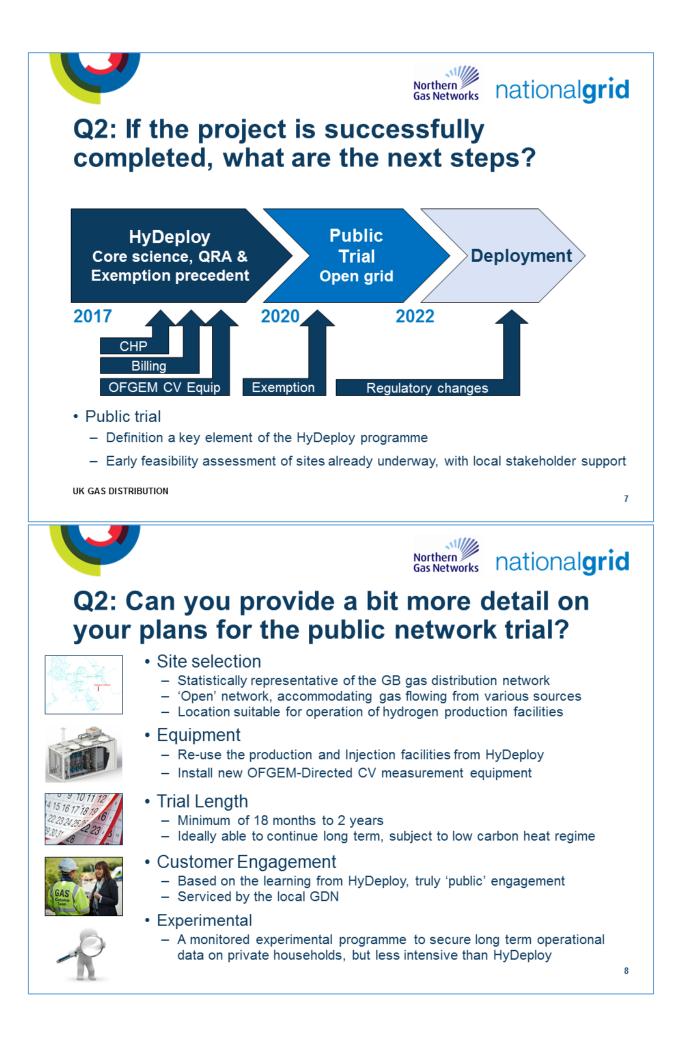
Trial Length: Minimum of 18 months to 2 years, although ideally it would be longer than this, although this would depend on specifics of site location, and whether there is an enduring support regime for low carbon heat by that stage.

Customer Engagement: This would be based on the HyDeploy learning, executed in a truly public environment. This would be serviced by the GDNs, rather than in conjunction with the university as is the case at Keele

Experimental: There would still be a need to undertake monitoring both on the network and, where possible, on appliances in private households, similar to the Oban project. It is important to understand in detail any differences between the work at Keele and on a public network. However, it is expected that this will be significantly less intensive that in the HyDeploy project due to the body of work which will already be developed.

In parallel, on the basis of successfully securing funding for the SEND programme, Keele University anticipates being able to support hydrogen training for gas fitters, as part of its activities to support businesses.

| Attachments | |
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| Project code | NGGDGN03/1 | Question Number | 14 | |
|---|---|--|------------------------------|--|
| Question date | 26-09-16 | Answer date | 04-10-16 | |
| Submission section question relates to | | | | |
| Торіс | | | | |
| Question | How sensitive are the costs and be price of natural gas? | enefits to changes in t | he future | |
| Notes on question | | | | |
| Answer | The following is a commentary support meeting on 30/09/16 shown below. | ing the slides used in th | ne bilateral | |
| | The price of natural gas flows into the assessment primarily for the tranche of Hydrogen generated using a Steam Methane Reformation unit with associated CCS. | | | |
| | In its Future Energy Scenarios, National Grid has forward gas curves for a high and low cases as well as the central. The high case is between 130-140% of the central case and the low is 82-88%, thus giving a wide spread for the purposes of reviewing sensitivity. As shown in the tables below, this does have an impact on the quantum of the savings, for example a central case of £8,060m savings varying from £7,084m to £8,502m with high and low gas prices respectively. However this does not change the fundamental conclusion. | | | |
| | It should also be noted that higher gas electricity prices (dispatchable gas gen annual grid generation in order to acco Therefore the cost of the heat pump re offset an element of the change shown | eration being likely to commodate fluctuating with the second sec | ontribute to ind and solar). | |
| Attachments | | | | |





Q3: How sensitive are costs and benefits to changes in the future price of natural gas?

| Wholesale gas (£/MWh) | 2015 | 2020 | 2030 | 2040 | 2050 | Range |
|--------------------------|------|------|------|------|------|----------|
| High Case | 14.6 | 20.6 | 27.3 | 27.3 | 27.3 | 130-140% |
| Base Case | 14.6 | 15.5 | 19.4 | 20.4 | 20.4 | Base |
| Low Case | 14.6 | 12.7 | 17.0 | 17.0 | 17.0 | 82%-88% |

Results

| Cumulative NPV, GB | To 2030 | To 2040 | To 2050 |
|---------------------|----------|----------|----------|
| Values, 20% Blend | £million | £million | £million |
| Central | 1,897 | 6,025 | 8,060 |
| High Gas | 1,885 | 5,503 | 7,084 |
| Low Gas | 1,901 | 6,242 | 8,502 |
| Cumulative NPV, GB | To 2030 | To 2040 | To 2050 |
| Values, 10% Blend | £million | £million | £million |
| Central | 855 | 2,548 | 3,269 |
| High Gas | 849 | 2,286 | 2,780 |
| Low Gas | 857 | 2,656 | 3,489 |
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- FES scenarios consider a wide range from the base case
- Whilst there is an impact on the quantum of saving, it doesn't change the fundamental conclusion
- Higher gas prices would have some impact on electricity price & therefore cost of heat pumps offsetting some of change 9

| Project code | NGGDGN03/1 | Question Number | 15 | |
|---|--|--|----------------|--|
| Question date | 26-09-16 | Answer date | 04-10-16 | |
| Submission section question relates to | | | | |
| Торіс | | | | |
| Question | How might the funding and success form the debate on the future of th | - | | |
| Notes on question | | | | |
| Answer | The following is a commentary supporting the slides used in the bilateral meeting on 30/09/16 shown below. | | | |
| | The Comprehensive Spending review confirmed the funding of the RHI scheme until March 2021. The current regime is subject to a range of modifications within the existing framework due to be implemented in April 2017. However, as shown by the recent consultation, these interim changes remain within the context of the UK's renewable Energy commitments and based on the suite of technologies already included within the RHI scheme. | | | |
| | There is universal agreement that addressing the carbon emissions within the heating sector will require ongoing policy intervention to meet our carbon budget obligations. However, the objective is expected to move from a renewables focus to a carbon focus. Therefore there will need to be an appropriately revised support regime post March 2021, in absence of implementation of a wider overhaul of carbon pricing in general. | | | |
| | This means that the scope of such an in than the technologies currently support DECC back within BEIS, it is likely that 'infrastructural view' where the valuabl gas network, are considered carefully. | ed. Particularly with the this could entail more a | e move of 1 | |
| | In order for any government departme able to undertake an Impact Assessme particular solutions. | | | |
| | The key outcome of the HyDeploy proje hydrogen-natural gas blending that is f | | | |

Understanding the quantum of the phenomena is fundamental to any impact assessment. HyDeploy will also provide an evidence base for the costs, particularly related to the network and its management that such an approach would entail. As discussed in the bid, other regulatory barriers will need to be addressed, such as those related to Directed Compositional measurements and billing regimes. These need to be understood when evaluating a new regime. Whilst not core to the blended hydrogen approach, this project will also provide valuable technical evidence regarding the feasibility of 100% conversion, to inform the wider hydrogen debate and the role it could provide more widely.

Any new scheme must follow seamlessly from the current RHI regime, otherwise a hiatus will jeopardise ability to meet the 5th carbon budget. As shown in the figure below, against a realistic development programme for implementation of new policy, the HyDeploy programme provides timely evidence.

Attachments

